

Teknologi batubara

Ferian Anggara

JADWAL KULIAH GEOLOGI BATUBARA
SM II TA 2014-2015
KULIAH KELAS B RABU (09.00-11.00, R 32)
KULIAH KELAS A JUMAT (14.00-16.00, R 33)

No	MATERI	Februari		Maret		April		Mei		Juni	
		19/2	26/2	5/3	12/3	19/3	26/3	2/4	9/4	16/4	23/4
1	Pendahuluan	DHA									
2	Pembentukan batubara (Mre)	DHA									
3	Pembentukan batubara (Dep. Env)			SSS							
4	Geokimia batubara & Perdobubaraan			DHA	DHA						
5	Patologi Batubara					DHA					
6	Analisa Batubara						DHA				
7	Ujian Tengah Semester										
8	Klasifikasi batubara							DHA			
9	Eksploasi Batubara							SSS	SSS	DHA	
10	Eksploasi Batubara									DHA	
11	Pemanfaatan Batubara & Limbahnya										
12	Ujian Akhir Semester										
13	Ujian Akhir Semester										

3 April Libur Wafat Isa Almasih
 1 Mei Libur Hari Buruh

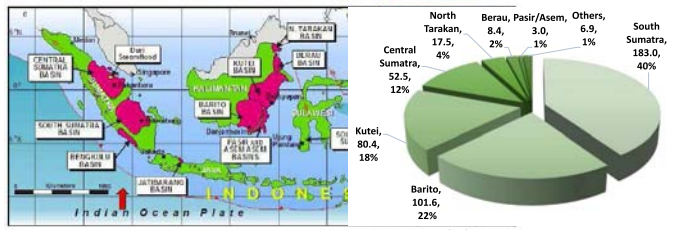
Outline

- Coal bed methane (CBM)
- Coal gasification
- Coal liquefaction
- Coal boiler and cooking coal

What is Coal Gas?

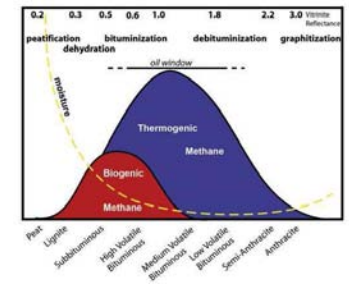
- This gas was considered one of the many **hazards** of coal mining
- **Recently**: unconventional resources
- Gas is generated during maturation of organic matter into coal and by microbes residing in a coal
- Coal deposits of all geologic ages have generated gas

Coal and CBM resources in Indonesia



Coal bed methane (CBM):
337-453 Trillion cubic feet

Schematic showing biogenic and thermogenic gas generation



Moore, 2012

Typical of CBM Production Curve

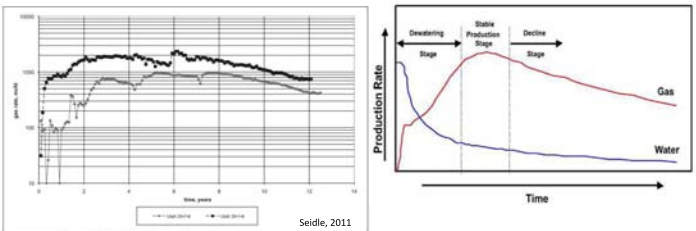


Fig. 1-3. Examples of slow negative decline—delta basin, Pennsylvanian

Conventional Gas Vs. CBM

Conventional Gas	Coalbed
Darcy flow of gas to wellbore.	Diffusion through micropores by Fick's Law.
Gas storage in macropores; real gas law.	Darcy flow through fractures.
Production schedule according to self decline curves.	Gas storage by adsorption on micropore surfaces.
Gas content from logs.	Initial negative decline.
Gas to water ratio decreases with time.	Gas content from cores. Cannot get gas content from logs.
Inorganic reservoir rock.	Gas to water ratio increases with time in latter stages.
Hydraulic fracturing may be needed to enhance flow.	Organic reservoir rock.
Macropore size: 1μ to 1 mm	Hydraulic fracturing required in most of the basins except the eastern part of the Powder River basin where the permeability is very high. Permeability dependent on fractures.
Reservoir and source rock independent.	Macropore size: $<5A^*$ to $50A^*$
Permeability not stress dependent.	Reservoir and source rock same.
Well interference detrimental to production.	Permeability highly stress dependent.
	Well interference helps production. Must drill multiple wells to develop.

Levine, 1990

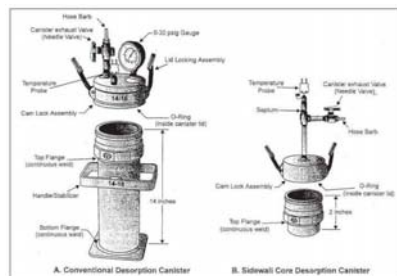
CBM-Outline

- Overview
- Adsorption (Gas content)
- Porosity
- Permeability (Cheat system)
- Gas Flow
- Reserve Analysis
- Dynamic reservoir
- Enhanced recovery

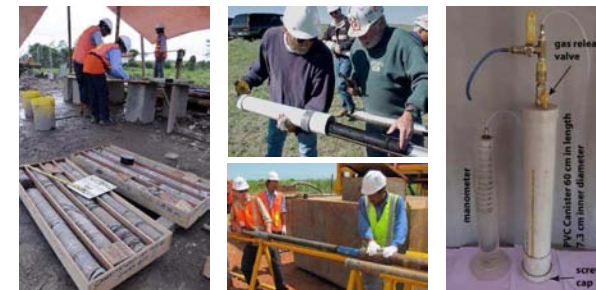
ADsorption vs ABSorption



Canister: Desorption test



Sampling

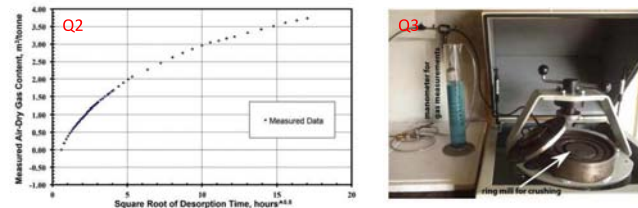


Gas desorption measurements

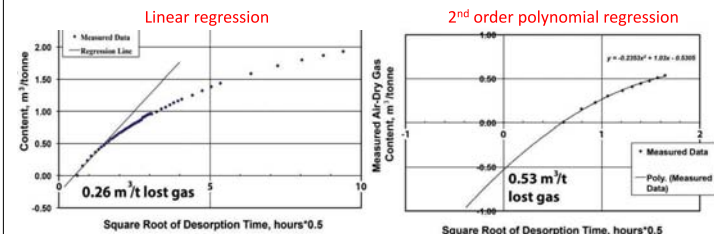
- 1. Lost gas (Q1)**
is the calculated amount of gas that has potentially been lost from the time the core leaves the reservoir at depth to when it is placed within a canister at the surface
- 2. Measured gas (Q2)**
the gas which is directly desorbed from the canister and measured using a manometer
- 3. Residual gas (Q3)**
 - After a sample is either 'fully' desorbed or when the operator decides that enough has been measured to achieve the desired goals of the sampling, the coal is removed from the canister
 - Crushing coal to approximately 250 μm size particles, which has gas tight seals and a gas lead from which the gas evolved can be removed for measurement.

$$\text{Total gas volume} = Q1 + Q2 + Q3$$

Q2 & Q3 calculation



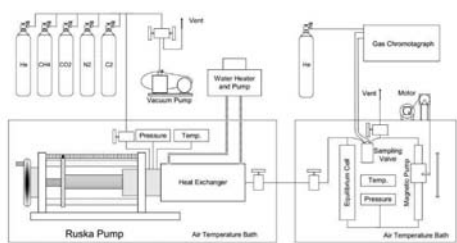
Q1 calculation



Adsorption test



PVT Apparatus, Kyushu University-Japan



Gasem et al., 2009

Adsorption test

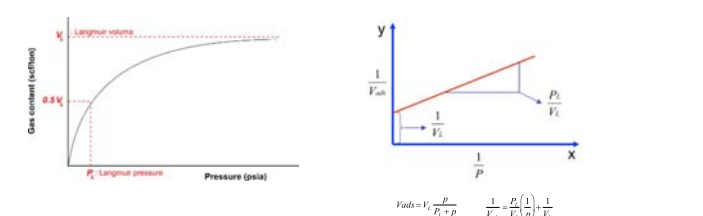
Client	Micah Global CDM	Gas	Methane
Sample	Brandon Basin Tondo Mine	Sample No	Ballo-20-7A
Location		Formation	Jasper Fm
		Depth (m)	410
		Sampling	3.5%
		Density (t/m³)	1.33

Adsorption Equation	
$V = \frac{V_{max} P}{P + P_0}$	
V - Gas content (m³/t)	
P - Pressure (kPa)	
V_{max} - Langmuir Volume (m³/t)	
P_0 - Langmuir Pressure (kPa)	

Test Summary	
Absolute Pressure (kPa)	Gas Adsorbed (m³/t)
101	Measured: 0.77
251	2.09
401	3.50
801	3.78
1401	4.07
2601	5.01
3401	5.67
4901	6.67

Isotherm Parameters		
Parameter	At Gauge Pressure	At Absolute Pressure
V_{max} - Langmuir Volume (m³/t)	6.59	7.56
P_0 - Langmuir Pressure (kPa)	971.72	976.49
Calculated gas content at 1 atm =	0.77	m³/t

Langmuir parameters



$$V_{ads} = V_L \frac{P}{P_L + P} = \frac{1}{\frac{1}{V_L} + \frac{1}{V_L} \left(\frac{1}{P_L} \right) + \frac{1}{V_L} \left(\frac{1}{P} \right)}$$

Gas saturation



- 1. **Desorption Isotherms**
 - ❖ "slow", "fast" or "in between"
 - ❖ reservoir temperature
- 2. **Adsorption Isotherms**
 - ❖ reservoir temperature
 - ❖ fresh samples!

$$\%g = 1 - ((a-d)/a) * 100$$

where,
 %g, is gas saturation
 a, is maximum gas holding capacity [adsorption]
 d, is total measured gas [desorption]

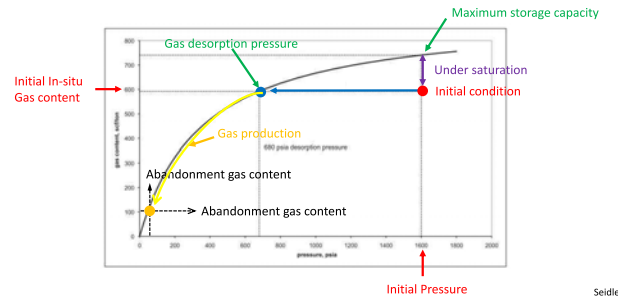
Moore, 2010



• But different types of coal can hold more or less gas (i.e. different coals have different holding capacities)

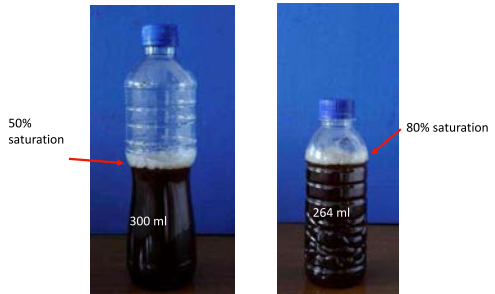
Moore, 2010

Gas saturation and desorption pressure



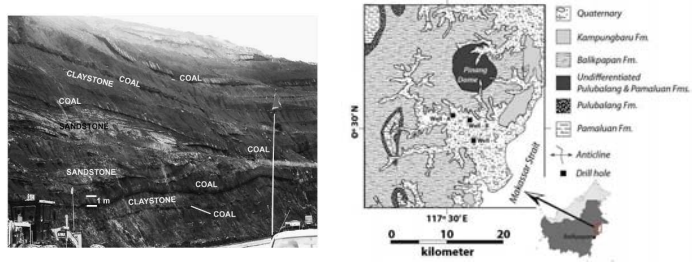
Seidle, 2011

Which deposit would you pick?



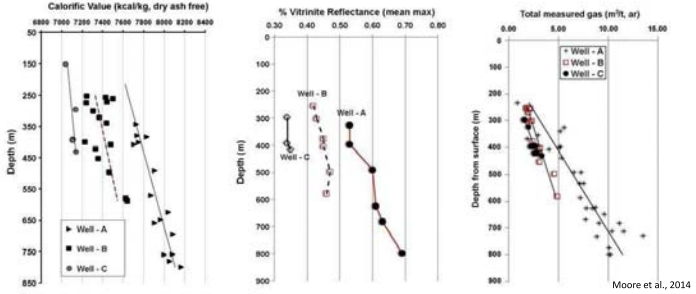
Moore, 2010

Coal properties & Gas content



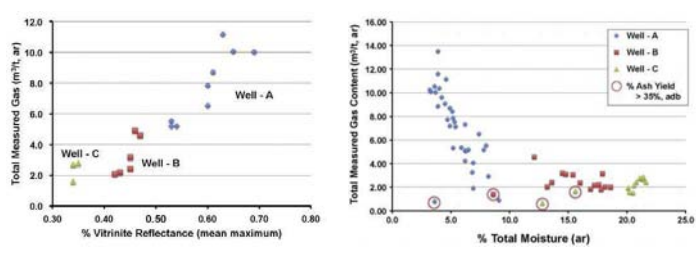
Moore et al., 2014

Coal properties & Gas content



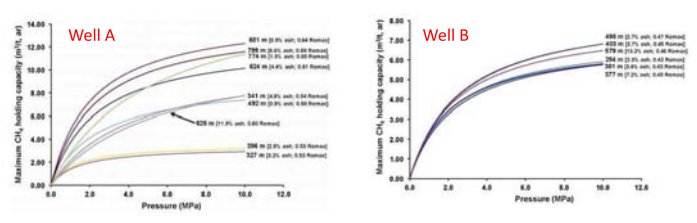
Moore et al., 2014

Coal properties & Gas content



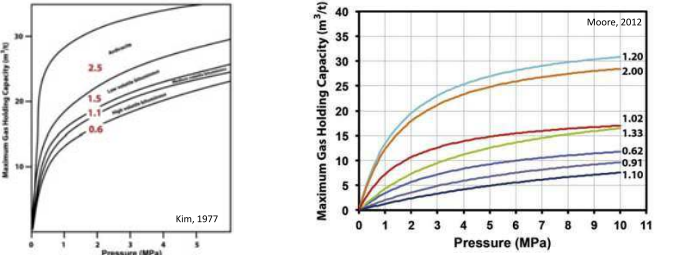
Moore et al., 2014

Adsorption isotherms



Moore et al., 2014

Adsorption isotherms related to rank



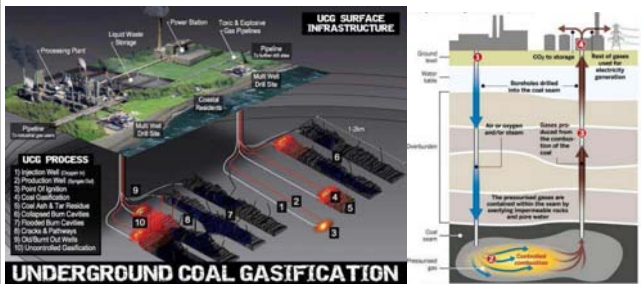
Rank-gas relationships shown are in general correct, they are far from universally observed

Gasification

- Proses pen-gas-an batubara (atau derivatifnya, mis. char) intinya adalah konversi bb menjadi gas yang *combustible* (dapat dibakar)
- Komposisi gas hasil gasifikasi: CO₂, H₂, CO₂, H₂O, CH₄, H₂S, H₂, CO (% vol.-nya bervariasi, tergantung macam2 faktor seperti peringkat bb, kandungan mineral, ukuran partikel pada saat diproses & kondisi reaksinya)
- Low Btu gas (150 – 300 Btu/scf), gasnya +- 50% nitrogen, sedikit H₂, CO, CO₂ & CH₄ -- umumnya produk insitu gasifikasi bb (tanpa ditambang dulu), bb hanya direaksikan dengan udara (oksidasi)
- Medium Btu gas (300 – 550 Btu/scf), gasnya terutama H₂ & CO, kadang CH₄ – prinsip sama dengan low btu, hanya oksidasinya dibuat dengan nitrogen barrier (mis. oksigen murni) supaya nitrogen tidak bercampur dalam sistem (nitrogen akan merendahkan nilai btu)
- High Btu gas (980 – 1080 Btu/scf), hampir semuanya CH₄ – pengasannya bisa dengan reaksi katalistik hidrogen & karbon monoksida (3H₂+CO→CH₄+H₂O), tapi kurang efisien. Cara lain bisa dengan hidrogasifikasi (C+2H₂ → CH₄).

Amijaya, 2015

Underground coal gasification

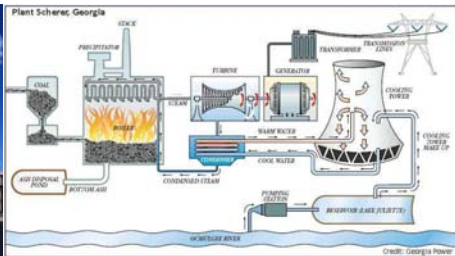
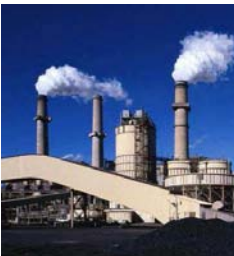


Liquifaction

- Prinsipnya melalui dekomposisi thermal bb (biasanya 400-500°C bb sudah/mulai mengeluarkan liquid)
- Proses secara kimiawi pada prinsipnya:
 - struktur kimia bb dipecah menjadi kecil-kecil, ikatan-ikatan organik dipecah menjadi lebih kecil
 - rasio atom H/C ditingkatkan (supaya menjadi liquid)
- Kadang disebut karbonisasi atau destructive distillation, tapi istilah ini tidak tepat karena proses karbonisasi tidak ditujukan untuk menghasilkan liquid sebagai produk utama (Corganik = Ccoke/char/carbon+liquid+gas)
- Metode: Pyrolysis, solvent extraction, catalytic liquefaction, indirect liquifaction

Amijaya, 2015

Coal boiler

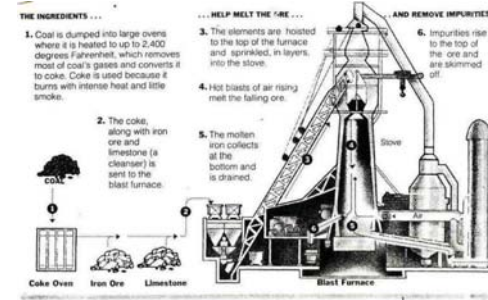


Coking Coals/Metallurgical Coals

- BB dengan karakteristik & diolah khusus yang dipakai dalam peleburan biji besi (dalam tanur).
- Hasil olahan BB ini disebut coke (residu solid karbon yang mengandung mineral).
- Dihasilkan dengan cara karbonisasi bb (dengan peringkat tertentu/hasil blending) dengan temperatur sd. 1400 K.
- Peran coke pada tanur:
 - Sebagai bahan bakar untuk reaksi kimia & peleburan slag & metal
 - Sebagai agen reduksi kimia karena menghasilkan gas untuk reduksi oksida besi
 - Sebagai penyangga (*permeable support*) biji besi, sehingga saat melebur, slag & besi dapat mengalir ke bawah dan gas dapat mengalir cerobong

Amijaya, 2015

Blast furnace



End